

**PROCESS FOR PRODUCING SYNGAS IN A SHORT CONTACT TIME REACTOR  
USING CATALYTIC PARTIAL OXIDATION OF HYDROGEN SULFIDE**

CROSS-REFERENCE TO RELATED APPLICATIONS

This application claims the benefit of provisional application no. 60/146,635 filed July 30, 1999, the disclosure of which is incorporated herein by reference.

STATEMENT REGARDING FEDERALLY SPONSORED  
RESEARCH OR DEVELOPMENT

Not applicable.

BACKGROUND OF THE INVENTION

Technical Field of the Invention

The present invention generally relates to processes for the catalytic oxidation of light hydrocarbons to synthesis gas (syngas), and more particularly to methods of increasing the yield of syngas in processes employing partial oxidation of methane or natural gas to products containing CO and H<sub>2</sub>. Still more particularly, the processes of the present invention relate to such methods in which the concurrent oxidation reaction (i.e., the complete combustion of methane to carbon dioxide and water) is replaced with combustion of hydrogen sulfide to sulfur and water, to improve the yield of synthesis gas.

Description of Related Art

Many refineries face an abundant supply of lower alkanes, i.e., C<sub>1</sub>-C<sub>4</sub> alkanes such as methane, and relatively few means of converting them to more valuable products. Much research has been devoted to investigating the conversion of methane to more easily transportable products. One technique that has been well-developed entails the partial oxidation

of light hydrocarbons in the presence of a catalyst. This technique results in the production of synthesis gas, *i.e.*, "syngas", a mixture of carbon monoxide and hydrogen. The catalytic partial oxidation of methane can be represented by the following reaction scheme:



- 5 At the same time, some of the methane burns completely, according to the equation:



Hence, syngas is typically a mixture of carbon monoxide and molecular hydrogen, generally having a hydrogen to carbon monoxide molar ratio in the range of 1:5 to 5:1, and which may contain other gases such as carbon dioxide.

- 10 Synthesis gas has utility as a feedstock for conversion to alcohols, olefins, or saturated hydrocarbons (paraffins) according to the well-known Fischer-Tropsch process, and by other means. Synthesis gas is not a commodity; instead, it is typically generated on-site for further processing. The uses for syngas include, but are not limited to, a feedstock for conversion to high molecular weight (*e.g.* C<sub>50+</sub>) paraffins, which in turn provide an ideal feedstock for hydrocracking, a feedstock for conversion to high quality jet fuel, and superior high octane value  
15 diesel fuel blending components. Another potential application of synthesis gas is for large-scale conversion to methanol.

- Syngas generation from methane typically takes place by one of three techniques. Steam reforming of methane is the most common, followed by partial oxidation, and autothermal  
20 reforming. Emerging technologies that have been developed to generate syngas from methane include a technique that entails exposing a mixture of methane and oxygen to a hot catalyst for a brief time, typically on the order of milliseconds or less, followed by cooling of the resultant gas stream. EP 303.438 describes a process for synthesis gas production by catalytic partial oxidation

to overcome some of the disadvantages and costs of steam reforming. A monolith catalyst is used with or without metal addition to the surface of the monolith and the process operates at space velocities of 20,000-500,000 hr<sup>-1</sup>. Conventional catalytic partial oxidation processes are also described in U.S. Patent Nos. 5,654,491 and 5,639,929, the disclosures of which are  
5 incorporated herein by reference.

Although in conventional syngas generation systems the syngas reaction is self-sustaining once initiated, it has been shown that 10 - 15 % of the carbon initially present as methane can be lost to the formation of CO<sub>2</sub> in combustion via equation (2) above. This directly reduces the yield of syngas that can be obtained. Hence, it is desirable to provide a syngas generation system  
10 that allows a better yield of carbon monoxide and hydrogen.

In a related aspect of petroleum refining, many petroleum feed streams and separated fractions contain sulfur. Sulfur is typically undesirable in most petroleum refining processes and products. Therefore, refineries typically upgrade the quality of the various petroleum fractions by removing the sulfur. Specifically, hydrodesulfurization units are used to break down the  
15 sulfur compounds in the petroleum fractions and convert the sulfur to H<sub>2</sub>S. In addition to hydrodesulfurization processes, other conversion processes in a typical refinery, such as fluid catalytic cracking, coking, visbreaking, and thermal cracking, produce H<sub>2</sub>S from sulfur containing petroleum fractions. The H<sub>2</sub>S from both the desulfurization processes and these conversion processes is typically removed from the gas streams or light liquid hydrocarbon  
20 streams using either chemical solvents based on alkanolamine chemistry or physical solvents. A circulating, regenerative H<sub>2</sub>S removal system employing an absorption stage for H<sub>2</sub>S pickup and a regeneration stage for H<sub>2</sub>S rejection produces a concentrated stream of H<sub>2</sub>S.

In conventional systems, this  $H_2S$  stream is then fed to a  $H_2S$  conversion unit, which converts the  $H_2S$  into a storable, saleable product such as elemental sulfur, sodium hydrosulfide solution, or sulfuric acid. Conversion of the  $H_2S$  to elemental sulfur is most common, mainly because elemental sulfur is the most marketable sulfur compound of those typically produced.

5 ~~The~~ process most commonly used to recover elemental sulfur from  $H_2S$  gas is the modified Claus sulfur recovery process. The conventional Claus process is well known in the art, and is also described in U.S. Pat. App. No. \_\_\_\_\_, filed concurrently herewith, entitled "*Process for Recovery of Sulfur From  $H_2S$  Using Short Contact Time Partial Oxidation*", the disclosure of which is incorporated herein by reference.

### SUMMARY OF THE INVENTION

10 The present invention provides a system that improves the yield of syngas generation by substituting  $H_2S$  partial oxidation for methane combustion in a syngas reactor. The partial oxidation of  $H_2S$  provides the heat necessary to sustain the syngas reaction at the desired temperature without consuming the methane. Hence, less methane is lost to complete

15 combustion and yield of the product is increased. One preferred embodiment provides the partial oxidation of  $H_2S$  in which  $H_2S$  is oxidized to give elemental sulfur and water. In this embodiment, the gases leaving the syngas generation system are treated further so as to increase the yield of elemental sulfur.

20 In accordance with the present invention, there is provided a method for improving the yield of a syngas generation system, comprising providing a first gas stream comprising a light hydrocarbon, mixing a second gas stream comprising  $H_2S$  with the first gas stream to form a feed gas stream, mixing the feed stream with an oxygen containing stream, then contacting the feed

gas stream with a hot catalyst to form a product stream, and removing syngas and elemental sulfur from the product stream.

The present invention also provides a method for improving the yield of a syngas generation system, comprising providing a first gas stream comprising a light hydrocarbon, mixing a second gas stream comprising  $H_2S$  with the first gas stream to form a feed gas stream, while maintaining said feed gas stream below 500 degrees C, contacting the feed gas stream with a hot catalyst to form a product stream wherein less than 10% of the light hydrocarbon is converted to carbon dioxide, and removing syngas and elemental sulfur from the product stream.

### BRIEF DESCRIPTION OF THE DRAWINGS

For a more detailed description of the present invention, reference will now be made to the accompanying drawings, wherein:

Fig. 1 is an enlarged cross-section of a reactor constructed in accordance with a preferred embodiment; and

Fig. 2 is a schematic diagram of the components of one preferred embodiment of the present system including the reactor of Fig. 1.

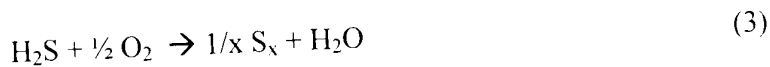
### DETAILED DESCRIPTION OF THE PREFERRED EMBODIMENTS

Several schemes for carrying out partial oxidation are known in the art. As discussed above, one scheme for carrying out the exothermic oxidation reaction entails a brief exposure of the methane feed to a hot catalyst followed by cooling the resultant gas stream. The hot catalyst is positioned in the flow path of the feed gas. The catalyst comprises a wire gauze, several layers of wire gauze, or a porous ceramic. The catalyst is designed so that only a first fraction of the

feed gas contacts the catalyst, while the balance of the gas serves to quickly cool the first fraction and prevent the oxidation reaction from proceeding too far.

According to the present invention, a stream of H<sub>2</sub>S is added to the feed stream of the syngas generation system. The feed stream comprises methane or a similar light hydrocarbon.

5 Pure oxygen is preferably mixed with the gas feed immediately before contacting the feed gases with a catalyst. Air, or a mixture of air and oxygen can be substituted for the pure oxygen. The H<sub>2</sub>S reacts with oxygen in the stream according to the reaction:



According to the present invention, H<sub>2</sub>S partial oxidation is incorporated into the syngas generation scheme as follows. Referring initially to Figure 1, a preferred embodiment of the  
10 present system includes a reactor 10 that includes feed injection openings 12, 14, and 16, a mixing zone 19, a reaction zone 20 and a cooling zone 30. Reaction zone 20 preferably includes a thermal radiation barrier 22 positioned immediately upstream of a catalytic device 24. Radiation barrier 22 is preferably a porous ceramic or refractory material that is suited to  
15 withstand operating temperatures and provide sufficient thermal insulation, such as are described in U.S. Patent 4,038,036 to Beavon, which is incorporated herein by reference in its entirety.

Catalytic device 24 is preferably a layer or layers of wire gauze 25 or a porous ceramic monolith (not shown) having a suitable catalyst supported on its surface. Gauze 25 is preferably one or more layers of a substantially planar, flexible woven metal-containing or metal-coated  
20 screen or gauze having about 20-120 mesh. More preferably, it is a gauze of metal wires about 25 micrometers to about 2.5 millimeters in diameter, which are made of about 87-93% by weight (wt-%) Pt and about 7-13 wt-% Rh. Alternative catalyst structures could include a disk with multiple perforations formed there through, a honeycomb-like structure, an etched foil and any

other structure that provides the desired amount of transparency to effect the desired partial oxidation. A detailed discussion of the catalyst structure and composition can be found in U.S. Patent No. 5,654,491 to Goetsch *et al.*, which is incorporated herein in its entirety.

5 Examples of suitable catalysts that can be included in the metal of the gauze or incorporated at its surface include, but are not limited to, platinum, rhodium, iridium, nickel, palladium, iron, cobalt, rhenium, rubidium, Pd-La<sub>2</sub>O<sub>3</sub>, Pt/ZrO<sub>2</sub>, Pt/Al<sub>2</sub>O<sub>3</sub>.

10 In operation, a light hydrocarbon, such as methane, is fed into one of the feed injection openings 12. H<sub>2</sub>S is fed into a second feed injection opening 14. Air or oxygen is fed into the third feed injection opening 16, which is preferably positioned close to catalyst 24. It will be understood that the feed injection openings can be configured differently from the configuration shown without affecting the principles or operation of the present system.

15 As the feed gases from feed injection openings 12, 14, 16 flow toward catalytic device 24, they are preferably subjected to thorough mixing by static mixer 18. During mixing, they are shielded by radiation barrier 22 from radiant heat that is generated downstream in the process. It is preferred that the temperature on the upstream side of barrier 22 be in the range of about 20°C to about 300°C. The feed gas stream is preferably at ambient temperature prior to contact with the catalyst. Preheating the feed gas stream is not desired, as it can cause homogeneous reactions and reduce the selectivity of the process of the present invention for the desired compounds. Therefore, preheating the feed gas mixture is typically avoided, although in some applications  
20 feed gas temperatures up to about 300° C can be tolerated.

After the gases pass barrier 22, they flow past catalytic device 24 and are simultaneously heated to an oxidation temperature in the range of from about 900 °C to about 1300 °C. The gas flow rate is preferably maintained such that the contact time for the portion of the gas that

contacts the catalyst is from about .001 to .01 seconds and more preferably from about .001 to .005 seconds.

This degree of contact produces a favorable balance between competing reactions and produces sufficient heat to maintain the catalyst at the desired temperature. Specifically, sulfur is produced by catalyzed partial oxidation according to equation (3) above, where x equals 2, 6, or 8, with x = 2 being the most likely. At the same time, exposure to the hot catalyst and oxygen partially oxidizes the hydrocarbons in the feed, according to the equation:



Oxygen for these reactions comes from the air, oxygen, or air/oxygen mix that is fed into the system with the H<sub>2</sub>S and hydrocarbon feed gases.

Typically, the catalyst structure is heated as a result of the exothermic chemical reactions occurring at its surface; however, it can additionally or alternatively be heated by external means, such as electrical resistance, magnetic induction, RF, etc. Heating by external means can allow for increases in the rate at which feed gas can be passed through the catalyst structure while still obtaining desirable reaction products. In many cases it is helpful to heat the catalytic device with external means at least at the start of the process, so as to initiate the exothermic reactions on the catalyst structure. This initial heating can be accomplished in any suitable manner including electrical resistance, magnetic induction, RF, or the like. Once the system is running, it is preferably is run adiabatically or nearly adiabatically (i.e., without loss of heat), so as to reduce the formation of carbon (e.g., coke) on the surface of the gauze catalyst.

According to the present invention, the rate of feed of H<sub>2</sub>S into the system is controlled and adjusted so that the heat generated by the oxidation of the H<sub>2</sub>S is sufficient to maintain the desired temperature in reaction zone 20 and thus reduce the amount of the light hydrocarbon that



is completely combusted. Hence, the mole ratio of  $H_2S$  to light hydrocarbon in the feed is preferably in the range of from about 1:10 to about 2:3. Where the light hydrocarbon is methane, a preferred ratio of  $H_2S$  to methane is 2:3.

The rapid heating of the feed gases as a result of contact with the hot catalyst promotes fast reaction rates. In accordance with the present invention, the feed gas stream velocity past catalyst structure 10 is preferably at least about 0.1 meter/second, often as high as 4-5 meters/second, and even as high as 70 meters/second. The maximum velocity will generally be determined by the specific equipment used; however, the theoretical limit is that velocity at which the reaction would be extinguished. If an external means of heating the catalytic device 24 is used, this theoretical limit is significantly large.

According to one preferred embodiment, the feed gas stream velocity is between about 0.1 and 100 meters/second. As a result, the superficial contact time of the feed gas stream with a preferred embodiment of gauze catalytic device 24 is less than about 10,000 microseconds, and typically within a range of about 1000-10,000 microseconds. When used in the present invention, it is preferred that the superficial contact time of the feed gas stream with the catalyst be less than about 5000 microseconds, more preferably less than about 2000 microseconds. Superficial contact time is inversely proportional to the term "space velocity" that is used in many chemical process descriptions.

Although for ease in comparison with prior art, space velocities at standard conditions have been used to describe the present invention, it is well recognized in the art that residence time is the inverse of space velocity and that the disclosure of high space velocities equates to low residence times.

From reaction zone 20, the reacted gases preferably enter a firetube boiler 40, where they are cooled to below 450 °C and preferably to below 340 °C. As shown, it is preferred that heat removed from the partially oxidized gases can be recaptured in steam heating or the like. The rapid cooling that occurs in the boiler drops the temperature to below about 450° C and thus ceases the above reactions. A detailed description of the considerations involved in operating a reactor using millisecond contact times is given in U.S. Patent No. 5,654,491, which is incorporated herein in its entirety.

Accordingly, and referring now to Figure 2, the present system preferably includes the, synthesis gas reactor 10, firetube boiler 40, a condenser 50, heater 55, a tailgas cleanup units 60,

a cooler, and a quench tower 80. The cooled, partially oxidized gases flow from boiler 40 into condenser 50, where they are cooled further until the dew point of the elemental sulfur is reached. This allows for the removal of elemental sulfur, as desired, from the process. Once the bulk of the elemental sulfur is removed, the partially oxidized gases are reheated in heater 55 and passed through a tailgas converter unit 60. Each tailgas converter unit 60 includes at least a sulfur absorbing material 56 in contact with the fluid. More specifically, in each converter unit 60, the hot gas stream is passed over a bed of zinc or iron oxide. In this bed, any elemental sulfur is converted to metal sulfide and retained in the bed.

The effluent from the sulfur absorber is then preferably cooled sufficiently to condense the bulk of any remaining water from the gas stream.

The treated gases, which comprise CO, hydrogen, and nitrogen, are then sent to a synthesis gas conversion unit such as a methanol plant or a Fischer-Tropsch plant.

By substituting the heat of the partial oxidation of H<sub>2</sub>S for the combustion of methane, the present invention provides the heat necessary to maintain the syngas reaction at the desired

temperature without giving up the methane to combustion products. This, in turn, results in a higher overall yield for the process.

While a preferred embodiment of the present invention has been shown and described, it will be understood that variations can be to the preferred embodiment, without departing from the scope of the present invention. For example, the mixing process can be altered or replaced  
5 with an active mixer, the thermal barrier can be modified, the structure and composition of the catalyst can be varied, and the tail gas treatment steps can be modified.

The complete disclosure of all patents, patent documents, and publications cited herein are incorporated by reference. The foregoing detailed description and examples have been given  
10 for clarity of understanding only. No unnecessary limitations are to be understood therefrom. The invention is not limited to the exact details shown and described, for variations obvious to one skilled in the art will be included within the invention defined by the claims.